

Simulation of surface accumulation of anthropogenic polydisperse aerosol

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A mathematical model of pollutant sedimentation on the surface is considered with allowance made for climatic characteristics. Transition probabilities are constructed based on the Fokker–Planck–Kolmogorov equation, which is solved numerically. Specific calculated results for Irkutsk are presented, and the influence of emissions from Irkutsk industrial plants on the water area of Southern Baikal is estimated.

Pollution of the environment with anthropogenic emissions has a negative effect on living organisms, soil, buildings, architectural monuments, and constructions. It causes metal corrosion and decreases atmospheric transparency. Under the effect of gravity, pollutants deposit onto the surface (soil, water bodies) from the atmosphere. Surface run-off causes secondary pollution of water bodies (partial washout of pollutants from soil). This is why estimation of pollutant flow from the atmosphere to the surface is of great importance. One of the means of such estimation is mathematical simulation that permits one to find the optimal variant from the viewpoint of minimizing anthropogenic load by simulating possible situations on a computer.

A light pollutant in a homogeneous medium is described in Refs. 1 and 2. In this paper, we consider a passive pollutant characterized by a certain sedimentation rate in an anisotropic medium. The diffusion equation for this pollutant has the form

$$\frac{\partial s}{\partial t} + \frac{\partial u_i s}{\partial x_i} - \frac{\partial w_g s}{\partial x_3} = F + \frac{\partial}{\partial x_i} v_{ij} \frac{\partial s}{\partial x_j}, \quad (1)$$

where s is the pollutant concentration; u_i is the component of medium velocity along the corresponding coordinate x_i ($i = \overline{1, 3}$); w_g is the gravitational sedimentation rate which is different for particles of different fractions; F is the intensity of pollutant sources; t is time; v_{ij} are the coefficients of turbulent diffusion. Repeating indices mean summation.

Let us represent s , u_i , v_{ij} , and F as a sum of mean values and deviations. Then Eq. (1) takes the form

$$\begin{aligned} \frac{\partial(\bar{s} + s')}{\partial t} + \frac{\partial(\bar{u}_i + u'_i)(\bar{s} + s')}{\partial x_i} - \frac{\partial w_g(\bar{s} + s')}{\partial x_3} = \\ = \bar{F} + F' + \frac{\partial}{\partial x_i} (\bar{v}_{ij} + v'_{ij}) \frac{\partial(\bar{s} + s')}{\partial x_j}. \end{aligned}$$

Transforming the right-hand side of the last equation, we obtain

$$\begin{aligned} \frac{\partial(\bar{s} + s')}{\partial t} + \frac{\partial(\bar{u}_i + u'_i)(\bar{s} + s')}{\partial x_i} - \frac{\partial w_g(\bar{s} + s')}{\partial x_3} = \\ = \bar{F} + F' + \frac{\partial \bar{v}_{ij}}{\partial x_i} \frac{\partial \bar{s}}{\partial x_j} + \bar{v}_{ij} \frac{\partial^2 \bar{s}}{\partial x_i \partial x_j} + \frac{\partial \bar{v}'_{ij}}{\partial x_i} \frac{\partial s'}{\partial x_j} + \bar{v}'_{ij} \frac{\partial^2 s'}{\partial x_i \partial x_j} + \\ + \frac{\partial v'_{ij}}{\partial x_i} \frac{\partial \bar{s}}{\partial x_j} + v'_{ij} \frac{\partial^2 \bar{s}}{\partial x_i \partial x_j} + \frac{\partial v'_{ij}}{\partial x_i} \frac{\partial s'}{\partial x_j} + v'_{ij} \frac{\partial^2 s'}{\partial x_i \partial x_j}. \end{aligned}$$

Let us now average the last equation using the properties of mean values:

$$\begin{aligned} \frac{\partial \bar{s}}{\partial t} + \frac{\partial \bar{u}_i \bar{s}}{\partial x_i} - \frac{\partial w_g \bar{s}}{\partial x_3} = \bar{F} - \frac{\partial \overline{u'_i s'}}{\partial x_i} + \\ + \frac{\partial \bar{v}_{ij}}{\partial x_i} \frac{\partial \bar{s}}{\partial x_j} + \bar{v}_{ij} \frac{\partial^2 \bar{s}}{\partial x_i \partial x_j}. \quad (2) \end{aligned}$$

As in Refs. 1 and 2, to construct the probability model, we turn to the second Kolmogorov equation written in the phase coordinate s :

$$\frac{\partial p}{\partial t} = - \frac{\partial}{\partial s} [A(t, s) p] + \frac{\partial^2}{\partial s^2} [B(t, s) p], \quad (3)$$

where $p = p(t, s)$ is the differential distribution law for

the parameter s ; $A = \frac{\partial \bar{s}}{\partial t}$ and $B = \frac{1}{2} \frac{\partial^2 \bar{s}}{\partial t}$ are respectively the mean rate of variation of the mean concentration and the intensity of random oscillations about this mean value in the interval $t \in [0, T]$.

The initial state is $p(0, s) = p_0(s)$. The boundary conditions are as follows:

$$\frac{\partial(Bp)}{\partial s} - Ap = 0 \text{ at } s \rightarrow \infty, \quad \int_0^\infty p(t, s) ds = 1. \quad (4)$$

The problems of solvability of Eqs. (3) and (4) under certain restrictions placed on the coefficients A and B were considered by Kolmogorov in Ref. 3. In particular, proofs were performed for the so-called Bachelier case when $A(t) = 0$ and $B(t) = 1$, i.e., the Kolmogorov equation is reduced to the classical equation of heat transfer (at $s = x$), for the case when the coefficient A varies linearly and B is an arbitrary constant, and for the case $A(t, x) = 0$ and $B(t, x) = x$.

The unknown values in Eq. (3) are p , A , and B . To close the equation, let us find A and B . To determine the coefficient A , we perform the following calculations. First, Eq. (2) is subtracted from Eq. (1):

$$\begin{aligned} & \frac{\partial s'}{\partial t} + \frac{\partial}{\partial x_i} (u_i s - \bar{u}_i \bar{s}) - \frac{\partial \omega_g s'}{\partial x_3} = \\ & = F' + \frac{\overline{\partial u'_i s'}}{\partial x_i} + \frac{\partial}{\partial x_i} \overline{v_{ij} \frac{\partial s}{\partial x_j}} - \frac{\partial \bar{v}_{ij}}{\partial x_i} \frac{\partial \bar{s}}{\partial x_j} - \bar{v}_{ij} \frac{\partial^2 s}{\partial x_i \partial x_j}. \end{aligned}$$

Transforming both sides of the last equation, we obtain

$$\begin{aligned} \frac{\partial s'}{\partial t} = & -u_i \frac{\partial s'}{\partial x_i} - u'_i \frac{\partial \bar{s}}{\partial x_i} - \left(\frac{\partial u'_i}{\partial x_i} + s' \frac{\partial u_i}{\partial x_i} \right) + \frac{\partial \omega_g s'}{\partial x_3} + \\ & + F' + \frac{\overline{\partial u'_i s'}}{\partial x_i} + \frac{\partial}{\partial x_i} \bar{v}_{ij} \frac{\partial s'}{\partial x_j} + \frac{\partial}{\partial x_i} \overline{v_{ij} \frac{\partial s}{\partial x_j}}. \end{aligned} \quad (5)$$

For an incompressible liquid, every summand in parentheses vanishes because it is divergence of the velocity field and its fluctuations.

Following Refs. 4 and 5, we can neglect the influence of a passive pollutant on the velocity field of the medium in the linear approximation, i.e., the turbulent velocity field is assumed to be independent of pollutant concentration. Let us introduce a designation

$$q_k = \overline{u'_i s'}, \quad (6)$$

where s' is unknown.

Further, as in Ref. 1, Eq. (5) is integrated from t to $t + \tau$, where $t \geq \tau$ (τ is the Eulerian time scale), in order to satisfy Eq. (6). Then both sides of the resulted equation are multiplied by $u'_k(t + \tau)$ and averaged within the interval $T - \tau$ ($T \gg \tau$):

$$\begin{aligned} q_k = & \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) s'(t + \tau) dt_1 = \\ & = \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) s'(t) dt_1 - \end{aligned}$$

$$\begin{aligned} & - \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} u_i \frac{\partial s'}{\partial x_i} dt_1 dt - \\ & - \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} u'_i \frac{\partial \bar{s}}{\partial x_i} dt_1 dt + \\ & + \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} \frac{\partial \omega_g s'}{\partial x_3} dt_1 dt + \\ & + \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} F' dt_1 dt + \\ & + \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} \frac{\partial \overline{u'_i s'}}{\partial x_i} dt_1 dt + \\ & + \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} \frac{\partial}{\partial x_i} \bar{v}_{ij} \frac{\partial s'}{\partial x_j} dt_1 dt + \\ & + \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} \frac{\partial}{\partial x_i} \overline{v_{ij} \frac{\partial (s + s')}{\partial x_j}} dt_1 dt. \end{aligned} \quad (7)$$

The first summand in the right-hand side of the last equation vanishes because the integrands $u'_k(t + \tau)$ and $s'(t)$ are not correlated. Further, let us use the method of recursive inclusions.^{4,5} As a result, we obtain the first approximation for Eq. (6):

$$\overline{u'_i s'}^{(1)} = -N_{ki}^{(1)} \frac{\partial \bar{s}}{\partial x_i} + Q^{(1)}, \quad (8)$$

where

$$\begin{aligned} N_{ki}^{(1)} = & \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} u'_i(t_1) dt_1 dt; \\ Q^{(1)} = & \frac{1}{T - \tau} \int_0^{T-\tau} u'_k(t + \tau) \int_t^{t+\tau} F'(t_1) dt_1 dt. \end{aligned}$$

Substituting Eq. (8) into Eq. (2), we obtain the closed equation for mean concentrations:

$$\begin{aligned} A = \frac{\partial \bar{s}}{\partial t} = & - \frac{\partial \bar{u}_i \bar{s}}{\partial x_i} + \frac{\partial \omega_g \bar{s}}{\partial x_3} + \bar{F} + \\ & + \frac{\partial}{\partial x_i} \left(N_{ij}^{(1)} \frac{\partial \bar{s}}{\partial x_j} - Q^{(1)} \right) + \frac{\partial}{\partial x_i} \bar{v}_{ij} \frac{\partial \bar{s}}{\partial x_j}. \end{aligned} \quad (9)$$

Thus, the equation for the coefficient A is derived.

Similarly, we can obtain the approximation of an arbitrary order. The error of the first approximation was estimated by comparison with analytical solutions (it does not exceed 20%).

To find the coefficient B , let us turn to Eq. (5). Multiply both its sides by $2s'$ and add to the equation of continuity of incompressible liquid (whose sides are pre-multiplied by s'^2). After averaging, in the first approximation we obtain

$$B = N_{ki}^{(1)} \left(\frac{\partial \bar{s}}{\partial x_i} \right)^2. \quad (10)$$

Pulsations of the sources F' are neglected in Eq. (10). This can be also done in Eq. (9).

The obtained coefficients A and B close Eq. (3). However, Eq. (9) for the coefficient A is also of interest, as it permits one not only to calculate the field of mean pollutant concentrations in commonly accepted ways at typical or averaged situations but also to take into account fluctuation effects of the medium.

The obtained closed equations (the Kolmogorov equation and that for the coefficient A) with the corresponding initial and boundary conditions are solved numerically in the Cartesian coordinate system using the method of fictitious areas, which allow calculations with an arbitrary function describing the relief. For time quantization, the Crank–Nicolson scheme and two-cycle multicomponent splitting method can be used.⁶

Without changing the essence of the matter, for brevity we write Eq. (9) in the form

$$\begin{aligned} \frac{\partial C}{\partial t} + \text{div}(\mathbf{V} C) = \Phi + \frac{\partial}{\partial x} K_x \frac{\partial C}{\partial x} + \\ + \frac{\partial}{\partial y} K_y \frac{\partial C}{\partial y} + \frac{\partial}{\partial z} K_z \frac{\partial C}{\partial z}, \end{aligned} \quad (11)$$

where $x = x_1$, $y = x_2$, and $z = x_3$ are the axes of the Cartesian coordinate system; x and y are directed horizontally, z is directed vertically upward; $C = \bar{s}$, $\mathbf{V} = \mathbf{v} - \mathbf{w}_g$, $\mathbf{v} = \mathbf{v} \{u = u_1, v = u_2, w = u_3\}$; $K_{ij} = N_{ij}^{(1)} + \bar{v}_{ij}$; $\Phi = \bar{F} - \frac{\partial}{\partial x_i} Q^{(1)}$ with the boundary conditions guaranteeing uniqueness of the solution:

$$C = C_0 \text{ at } t = 0;$$

at the lower boundary

$$w_g C + N_z \frac{\partial C}{\partial z} = \beta C - \Phi_0$$

for $z = \Delta$; at other boundaries, either (a) $C = C_b$ or (b) $C = C_b$ for $V_n < 0$,

$$\frac{\partial C}{\partial x} = \frac{\partial C}{\partial y} = \frac{\partial C}{\partial z} = 0 \text{ for } V_n \geq 0, \quad (12)$$

where C_b is the background concentration; V_n is the projection of the velocity vector onto the external normal to the boundary surface; β is the coefficient describing the interaction between the pollutant and the surface.

Let us consider the method for solving the problem presented by Eqs. (11) and (12). Since the antisymmetric form of the operator is preferable when constructing energetically balanced finite-difference approximations, Eq. (11) is transformed, using the equation of continuity for the incompressible atmosphere, to the following form:

$$\begin{aligned} \frac{\partial C}{\partial t} + \frac{1}{2} (\mathbf{V} \text{grad } C + \text{div} (C \mathbf{V})) = \\ = \frac{\partial}{\partial x} K_x \frac{\partial C}{\partial x} + \frac{\partial}{\partial y} K_y \frac{\partial C}{\partial y} + \frac{\partial}{\partial z} K_z \frac{\partial C}{\partial z} + \Phi. \end{aligned}$$

Let us introduce a nonuniform grid with main nodes $x_i = i \Delta x$ ($i = 0, 1, \dots, I + 1$), $y_j = j \Delta y$ ($j = 0, 1, \dots, J + 1$), $z_k = \Delta z_k$ ($k = 0, 1, \dots, K + 1$), and $t_n = n \Delta t$ ($n = 0, 1, \dots$) and the steps Δx , Δy , Δz_k , and Δt . We also use auxiliary points $x_{i+1/2}$, $y_{j+1/2}$, $z_{k+1/2}$ situated at the center of the main intervals. Let us designate

$$\begin{aligned} C_{i,j,k}^n &= C(x_i, y_j, z_k, t_n); \Delta_k = (\Delta z_{k+1} + \Delta z_k) / 2; \\ u_{i+1/2,j,k} &= (u_{i+1,j,k} + u_{i,j,k}) / 2; \\ v_{i,j+1/2,k} &= (v_{i,j+1,k} + v_{i,j,k}) / 2; \\ w_{i,j,k+1/2} &= (w_{i,j,k+1} + w_{i,j,k}) / 2. \end{aligned}$$

The finite-difference analogs of the operators are the following:

$$\begin{aligned} (L_1^n C)_{i,j,k} &= \frac{u_{i+1/2,j,k}^n C_{i+1,j,k} - u_{i-1/2,j,k}^n C_{i-1,j,k}}{2\Delta x} - \\ &- \frac{1}{\Delta x^2} [K_{x_{i+1/2,j,k}}^n (C_{i+1,j,k} - C_{i,j,k}) - \\ &- K_{x_{i-1/2,j,k}}^n (C_{i,j,k} - C_{i-1,j,k})], \\ (L_2^n C)_{i,j,k} &= \frac{v_{i,j+1/2,k}^n C_{i,j+1,k} - v_{i,j-1/2,k}^n C_{i,j-1,k}}{2\Delta y} - \\ &- \frac{1}{\Delta y^2} [K_{y_{i,j+1/2,k}}^n (C_{i,j+1,k} - C_{i,j,k}) - \\ &- K_{y_{i,j-1/2,k}}^n (C_{i,j,k} - C_{i,j-1,k})], \\ (L_3^n C)_{i,j,k} &= \frac{(w_{i,j,k+1/2}^n - w_g) C_{i,j,k+1} - (w_{i,j,k-1/2}^n - w_g) C_{i,j,k-1}}{2\Delta_k} - \\ &- K_{z_{i,j,k+1/2}}^n \frac{C_{i,j,k+1} - C_{i,j,k}}{\Delta z_{k+1} \Delta_k} + K_{z_{i,j,k-1/2}}^n \frac{C_{i,j,k} - C_{i,j,k-1}}{\Delta z_k \Delta_k}. \end{aligned}$$

Using the Crank–Nicolson scheme at every fractional step $[t_n, t_{n+1}]$, we can write the splitting algorithm in the form

$$\begin{aligned} \left(E + \frac{\Delta t}{2} L_m^n \right) C^{n+m/4-1} = \left(E - \frac{\Delta t}{2} L_m^n \right) C^{n+(m-1)/4-1}, \\ m = 1, 2, 3; \\ C^{n+1/4} = C^{n-1/4} + \Delta t \Phi^n; \end{aligned}$$

$$\left(E + \frac{\Delta t}{2} L_{5-m}^n\right) C^{n+m/4} = \left(E - \frac{\Delta t}{2} L_{5-m}^n\right) C^{n+(m-1)/4},$$

$$m = 2, 3, 4,$$

where E is the unit matrix.

The difference approximation of the problem (3) and (4) is also constructed based on the Crank–Nicolson scheme. Let us designate

$$s_\gamma = \gamma \Delta s_\gamma \quad (\gamma = 0, 1, 2, \dots, \Gamma + 1),$$

$$\Delta s_{\gamma+1} = s_{\gamma+1} - s_\gamma, \quad ss_\gamma = (ds_\gamma + ds_{\gamma+1})/2,$$

$$(\Lambda^n p)_\gamma = \frac{A_{\gamma+1}^n p_{\gamma+1} - A_{\gamma-1}^n p_{\gamma-1}}{2ss_\gamma} - \frac{B_{\gamma+1}^n p_{\gamma+1} - B_\gamma^n p_\gamma}{ss_\gamma ds_{\gamma+1}} -$$

$$- \frac{B_\gamma^n p_\gamma - B_{\gamma-1}^n p_{\gamma-1}}{ss_\gamma ds_\gamma} \quad (\gamma = 0, 2, \dots, \Gamma - 1).$$

The boundary condition p_0 is determined from the condition of fulfillment of the probability measure (4) by the trapezium rule.

At the right boundary of the integration domain

$$(\Lambda^n p)_\Gamma = \frac{A_{\Gamma-1}^n p_{\Gamma-1}}{2ss_\Gamma} + \frac{B_\Gamma^n p_\Gamma}{ss_\Gamma ds_{\Gamma+1}} - \frac{B_\Gamma^n p_\Gamma - B_{\Gamma-1}^n p_{\Gamma-1}}{ss_\Gamma ds_\Gamma}.$$

Thus, the finite-difference approximation has the form

$$\left(E + \Lambda^n \frac{\Delta t}{2}\right) p^{n+1} = \left(E - \Lambda^n \frac{\Delta t}{2}\right) p^n.$$

These finite-difference schemes are absolutely stable, and they are second-order approximations with respect to time and coordinates.

For numerical realization of the finite-difference equations, nonmonotonic simulation run⁷ is used.

Thus, Eq. (9) describes the dynamics of mean pollutant concentrations with allowance for fluctuations of input meteorological information, and Eq. (3) estimates the probability of these concentrations (including the excess above the given norms) for the considered time interval and permits us to calculate the flow Π of pollutants onto the surface:

$$\Pi = \sum_{i=1}^k s_i w_{gi},$$

where k is the degree of particle dispersion.

Numerical solutions were tested at the simplifications, which were used in the known analytical solutions. Besides, the calculated results were compared with the data obtained from processing of samples of stable snow cover.

Let us consider particular estimates of sedimentation of solid particles onto the surface. It is well-known that aerosols emitted by anthropogenic sources are considerably polydisperse, and the polydisperse structure determines their physical properties. A particle size distribution is usually

described as a part (per cent) df of particles whose radii lay in the interval $(r, r + dr)$, i.e., $df = f(r)dr$, under the condition that the particle size distribution function has the property

$$P(0 < r < \infty) = \int_0^\infty f(r)dr = 1.$$

Usually, the part of aerosols particles, whose radii lay within finite intervals, is experimentally determined, i.e., histograms are obtained instead of continuous probability curves. However, emissions are nonstationary in practice, and thus it is impossible to determine the particle size distribution exactly. So, the distribution is approximated by some analytical law. Theoretically, we can derive an equation describing all aerodisperse systems. However, this equation would contain a great number of coefficients, and the fit of these coefficients for every system would not be expedient. This is why the proposed equations contain as small number of coefficients as possible. As a rule, two coefficients are used: particle size and the degree of aerosol polydispersity. The Roller and Rozin–Rammler equations etc.⁸ are examples.

Kolmogorov⁸ showed that, proceeding from simple hypotheses about the character of breaking of solid particles, it can be proved that the particle size distribution asymptotically tends to the lognormal distribution as particles become finer. That is why we used the lognormal law to calculate the distribution of solid particles emitted by Irkutsk power plants into the atmosphere. Dusting of ash dumps, open pits, and other plants was ignored in our calculations. There are more than 300 boiler houses in Irkutsk, and 97% of them have smoke stacks from 8 to 35 m high. The diameter of emitted particles is $\leq 4 \cdot 10^{-5}$ m, and the average density is 2800 kg/m³. The gravitational sedimentation rate was calculated for every fraction by the Stokes equation

$$w_g = (2\rho_n g r_n^2)/(9\mu),$$

where g is the free fall acceleration; μ is dynamic viscosity of the medium; ρ_n and r_n are density and radius of the particles. The gravitational sedimentation rate (calculated by the Stokes equation) ranges from 0.001 to 0.2 m/s depending on the particle size.

More than 80 000 kg/km² of pollutants deposit annually onto the underlying surface in the north-western part of Irkutsk (Fig. 1). This is the most polluted district of the city. In the south-western district, Novo-Irkutskaya power station provides the most part of thermal power. The smoke stacks of this station are 180 and 250 m in height. Therefore, its emissions are in the atmospheric boundary layer. Only large particles deposit near the station; other particles are transported very far by air flows. Figure 2 shows the estimate of annual accumulation of heavy particles (emitted by Irkutsk power plants) on the surface of Southern Baikal.

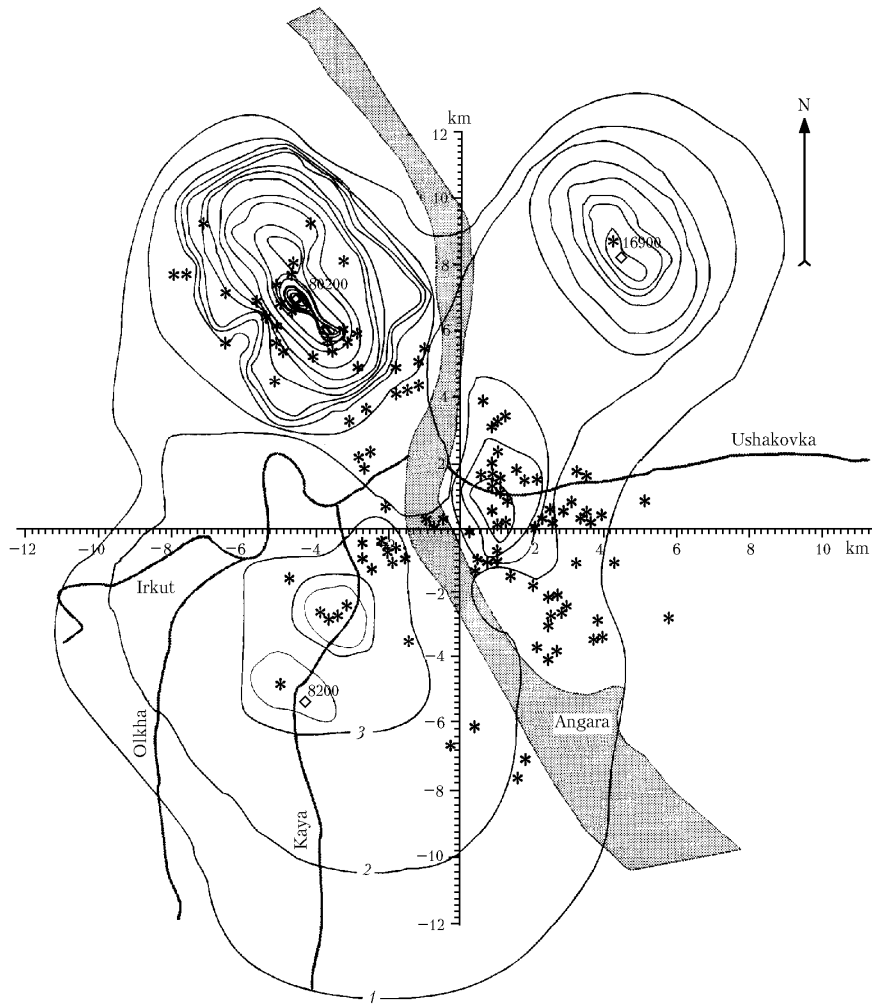


Fig. 1. Accumulation of an anthropogenic polydisperse pollutant on the underlying surface in Irkutsk during a year: pollutant sources (*); local maximums (). The isoline 1 corresponds to 2000 kg/km². Isoline step is 2000 kg/km².

96	134	196	306	524	1*	2*	9*	0	15*	4*	1*	998	603	396	276	202	153	119	94	77	63	53	45	38	33	28	25
89	123	181	284	483	951	2*	8*	17*	7*	3*	1*	895	571	388	277	226	157	123	99	80	66	56	47	40	35	30	26
79	109	157	239	392	717	1*	3*	4*	3*	1*	1*	735	504	359	265	201	156	124	100	82	68	57	49	42	36	31	28
69	92	127	187	293	485	951	1*	1*	1*	1*	363	578	424	318	244	190	151	122	100	83	69	58	50	43	37	32	28
57	75	103	147	216	363	574	843	959	870	726	573	447	300	274	218	174	142	117	97	81	69	58	43	38	33	29	
48	63	84	115	168	259	393	409	558	547	489	417	345	224	233	181	156	131	110	93	79	67	58	58	43	38	33	30
41	52	68	91	131	186	253	321	357	364	341	308	268	230	196	166	141	118	102	87	76	65	56	49	43	38	33	30
35	44	56	75	103	137	179	219	243	256	247	231	210	186	164	143	124	108	93	81	71	62	54	48	42	37	33	30
30	37	47	62	81	104	132	157	174	185	185	177	166	152	137	122	109	96	85	75	66	58	52	46	41	36	33	29
26	32	40	51	65	81	100	117	130	138	141	139	133	124	115	105	95	85	77	68	61	55	49	44	39	35	32	29
23	28	34	42	52	64	77	90	99	106	110	110	107	103	97	90	83	76	69	63	56	51	46	43	38	34	31	28
20	24	29	36	43	52	61	70	78	84	87	89	88	85	81	77	72	67	62	56	52	47	43	39	36	33	30	27
18	21	25	30	36	43	50	56	62	67	71	72	72	71	69	66	63	59	55	51	47	44	40	37	34	31	29	26
16	18	22	26	30	35	41	46	51	55	58	60	60	60	59	57	55	52	49	46	43	40	37	34	32	29	27	25
14	16	19	22	26	30	34	38	42	46	48	51	51	51	50	49	48	46	44	41	39	37	34	32	30	28	26	24
12	14	17	19	22	25	29	32	35	48	40	42	43	43	43	43	42	41	39	37	36	34	32	30	28	26	24	23
11	13	15	17	19	22	24	27	30	32	34	36	37	37	38	37	37	36	35	34	32	31	29	28	26	25	23	22
10	11	13	15	17	19	21	23	25	27	29	30	32	32	33	33	32	32	31	30	29	28	27	26	24	23	22	21
9	10	12	13	15	16	18	20	22	23	25	26	27	28	29	29	29	28	28	27	26	26	25	24	23	21	20	19
8	9	10	12	13	14	16	17	19	20	22	23	24	25	25	25	25	25	25	25	24	23	23	22	21	20	19	18

Fig. 2. Accumulation of an anthropogenic pollutant (kg/km²) on the underlying surface of Southern Baikal during a year; * is the order of the number 10³.

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